

## Research Article

# Nickel-phenanthroline Complex Supported on Mesoporous Carbon as a Catalyst for Carboxylation under CO<sub>2</sub> Atmosphere

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## Abstract

Carbon dioxide is a highly potential renewable C<sub>1</sub> source for synthesis of fine chemicals. Utilization of CO<sub>2</sub> in carboxylation reactions requires catalysts, such as: nickel complex for CO<sub>2</sub> activation. However, the use of homogeneous catalysts in the reaction is still less efficient due to the difficulty of separating the product and catalyst from reaction mixture. Therefore, it is necessary to heterogenize the nickel complex in a solid support such as mesoporous carbon. In this report, mesoporous carbon (MC) prepared from phloroglucinol and formaldehyde through soft template method was used as a solid support for Ni-phenanthroline complex (Ni-phen). The catalyst was characterized by Fourier Transform Infra Red (FT-IR), X-Ray Diffraction (XRD), Scanning Electron Microscope - Energy Dispersive X-Ray (SEM-EDX), and Surface Area Analyzer (SAA). The result of SAA characterization showed that the pore diameter of MC was 6.7 nm and Ni-phen/MC was 5.1 nm which indicates that the materials have meso-size pores. Ni-phen/MC material was then used as a heterogeneous catalyst in the carboxylation reaction of phenylacetylene under an ambient CO<sub>2</sub> pressure. The reactions were carried out in several variations of conditions such as temperature, time and catalyst types. Based on the results of the reaction, the best conditions were obtained at 25 °C for 8 h of reaction time using Ni-phen/MC catalyst.

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**Keywords:** carboxylation; CO<sub>2</sub>; mesoporous carbon; nickel complex; phenanthroline

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## 1. Introduction

Carbon dioxide (CO<sub>2</sub>) is a greenhouse gas which is quite abundant in nature and belongs to a non-flammable gas. CO<sub>2</sub> has the potential to become a renewable C<sub>1</sub> source for the synthe-

sis of useful chemicals given its high abundance as well as its low price [1]. To date, the most widely used carbon resources in the production of fine chemicals are obtained from conventional sources such as crude oil, natural gas, and coal [2]. Thus, utilization of CO<sub>2</sub> in this field is a promising and attractive method to continue to be developed. However, the use of CO<sub>2</sub> as a carbon resource has several obstacles due to its in-

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ert nature and low reactivity. In fact, most reactions involving CO<sub>2</sub> requires stoichiometric amounts of catalysts or harsh reaction conditions. Therefore, the development of a new and efficient catalytic system for the chemical transformation of CO<sub>2</sub> is one of the interesting topics in modern organic synthesis [3].

Nickel is a transition metal that has been widely used as catalyst for various transformations both in organic and inorganic reactions. In addition, nickel complexes have been widely employed as homogeneous catalyst in carboxylation reaction of various substrates with CO<sub>2</sub> [4]. The reaction occurs through formation of a C–C bond to produce a carboxylic acid or its derivatives. For example, carboxylation reaction of aryl and vinyl chloride with CO<sub>2</sub> using Ni complex catalysts was reported by Fujihara *et al.* [5]. The reactions were conducted with an atmospheric CO<sub>2</sub> at room temperature in the presence of Mn powder as a reducing agent. The reaction system gave good yield of product and is suitable for various types of aryl chloride. A double carboxylation reaction of alkynes with CO<sub>2</sub> using Ni complex catalyst was also reported by the same research group [6]. The reaction was conducted also in an atmospheric CO<sub>2</sub> gas in the presence of Zn powder as a reducing agent and MgBr<sub>2</sub> as an additive to facilitate the second insertion of CO<sub>2</sub>. Various aliphatic alkynes were suitable as the substrate for the double carboxylation giving a substituted maleic anhydride as the product. Similar system was also reported to be suitable for hydrocarboxylation of ynammides as substrate in the presence of small amount of water as proton source to give an  $\alpha$ -carboxylation product as a major product [7]. Whereas the presence of organozinc as reducing agent in the Ni-catalytic system gave  $\beta$ -carboxylation compound as the product for the same type of substrate [8].

It is known that a homogeneous catalyst has the advantage in the reaction process since the reactants and the catalyst being in the same phase and the reaction occurs in all phases. Thus, in most cases, homogeneous catalyst shows higher activity than the heterogeneous for the same reaction. However, homogeneous catalysis system has several drawbacks such as the need for additional costs for separation of product from the catalyst and reaction mixture, the short lifetime of the catalyst (difficult to recover) and the relatively expensive price of the catalyst itself. Therefore, the use of heterogeneous catalysts is becoming more desirable especially for applications on an industrial scale.

Mesoporous carbon is a class of porous nanomaterials having large pore size, which are around 2–50 nm [9]. The research of mesoporous carbon has long been carried out with various precursors such as sucrose [10], furfuryl alcohol [11], phenolic resin [9,12], glycerol [13], and gelatin [14]. It is known that mesoporous carbon shows some unique properties such as a controllable structure and pore size, high surface area, and high thermal and chemical stability. Thus, mesoporous carbon promises to be used as a supporting solid for heterogenization of nickel complex. The forming heterogeneous nickel complex could then be explored its activity in carboxylation reaction employing CO<sub>2</sub> as a C<sub>1</sub> carbon source. On our previous report, we succeeded the synthesis of Ni metal supported on mesoporous carbon [15]. However, the Ni/MC catalyst was not effective for carboxylation reaction under an atmospheric CO<sub>2</sub> pressure. We speculated that the limited exposure to the Ni metal as the active site causes the low catalytic activity of the catalyst system. Therefore, the use of complex nickel species supported on MC is expected to provide better catalytic activity since it has more exposed sides, thus it can interact with the reactants better.

In this research, we prepared the mesoporous carbon by soft template method, and then used as solid support for heterogenization of nickel-phenanthroline complex. We then explored the catalytic activity of the Ni-phen/MC for carboxylation reaction of phenylacetylene in an atmospheric CO<sub>2</sub>. Prior to catalytic activity, we also investigated the adsorption ability of the material towards CO<sub>2</sub>.

## 2. Materials and Methods

### 2.1 Materials

All materials were used in the experiments without additional purification. Phloroglucinol 99%, ethanol 99.8%, hydrochloric acid (HCl) 37%, and formaldehyde 37% were provided by Merck, while Pluronic F-127, 1,10-phenanthroline 98%, Ni(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O, magnesium bromide 98%, Zn powder, DMF 99.8%, and phenylacetylene 98% were obtained from Sigma Aldrich. Ultrahigh pure N<sub>2</sub> and CO<sub>2</sub> gases were used for carbonization and carboxylation, respectively, and were purchased from CV Retno Gas.

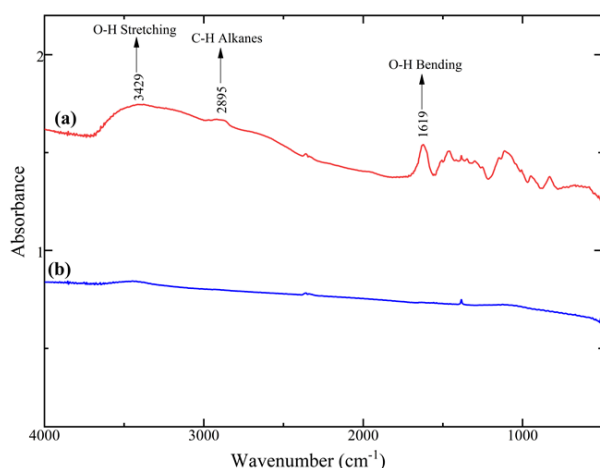
### 2.2 Synthesis of Mesoporous Carbon (MC)

Mesoporous carbon was synthesized using a previously reported procedure [9]. Briefly,

6.2595 g phloroglucinol precursor and 6.286 g Pluronic F-127 were dissolved in ethanol:water (25.6 : 22.6 mL) (w/w) solution and stirred vigorously at room temperature. After a complete copolymer dissolution, 0.4 mL HCl 37% (w/w) was added, and the solution was vigorously stirred for 30 min. Under continuous stirring, 6.25 mL formaldehyde 37% was added to the mixture. Then, the mixture was stirred for another 2 hours until being separated into two layers followed with decantation process to separate residue and filtrate. Then monolith (the bottom layer) was transferred to an autoclave for hydrothermal process in an oven at 100 °C for 24 hours. The resulting material was carbonized with a tubular furnace under the stream of N<sub>2</sub> gas with a heating rate of 1 °C/min from 100 to 400 °C and 5 °C/min from 400–850 °C before kept at 850 °C for 2 hours. The synthesized mesoporous carbon was characterized with FTIR (Shimadzu IR Prestige 21), XRD (PANalytical X'Pert PRO), SEM-EDX (JEOL JED-2300 Analysis Station), and SAA (Quantachrome Quadrasorb-Evo Surface Area and Pore Size Analyzer).

### 2.3 Immobilization of Ni-phenanthroline Complex to MC (Ni-phen/MC)

First, 0.3064 g 1,10-phenanthroline and 0.4954 g Ni(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O were dissolved in 4 mL deionized water (w/w) at room temperature. Under continuous stirring, 2 g mesoporous carbon was slowly added to the solution. The mixture was stirred for 6 hours followed with ultrasonication for 10 min. The mixture was further stirred at room temperature for 24 hours and then dried in an oven at 60 °C for 12 hours.



**Figure 1.** The spectrum of (a) monolith before carbonization, and (b) MC after carbonization.

### 2.4 Adsorption of Carbon Dioxide (CO<sub>2</sub>)

Carbon dioxide adsorption test was done following previously reported procedure [16]. CO<sub>2</sub> gas was flown into the chamber containing a 0.1 g sample (MC or Ni-phen/MC) with a flow rate of 50 cm<sup>3</sup>/min, at a pressure of 1 bar with various time (5, 10, and 15 min). The unadsorbed CO<sub>2</sub> gas was collected in 100 mL 0.1 M NaOH solution at the temperature of ±2 °C. Quantitative analysis of the amount of CO<sub>2</sub> in the solution was done using a titration method. 10 mL 0.1 M NaOH solution was titrated with 0.1 M HCl. The titration was conducted using phenolphthalein and methyl orange indicator to detect the first and second equivalent points.

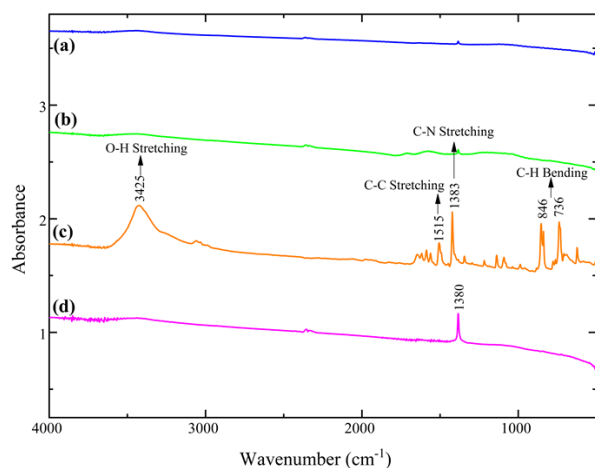
### 2.5 Carboxylation Reaction of Phenylacetylene with CO<sub>2</sub>

The carboxylation reaction was conducted in a glass reactor connected to a CO<sub>2</sub> gas balloon. The procedure adopted previously reported method [15,17]. To the reactor was added 0.0654 g Zn powder, 0.1841 MgBr<sub>2</sub>, 0.011 g Ni-phen/MC as a catalyst, 4 mL DMF as a solvent and 0.112 mL phenylacetylene as the substrate. Then the reactor was connected to a CO<sub>2</sub> balloon, and the mixture was stirred at a certain temperature (25, 50, and 75 °C) for a specified time (4, 8, and 16 hours). The carboxylation reaction was also conducted using MC (or Ni-phen complex) in place of Ni-phen/MC as comparison. After the reaction, 1 mL HCl 10% was added to the mixture and was stirred for 10 min followed with filtration to separate residue and filtrate. The carboxylation product as well as the unreacted phenylacetylene were analyzed by HPLC with Diamonsil C18 column.

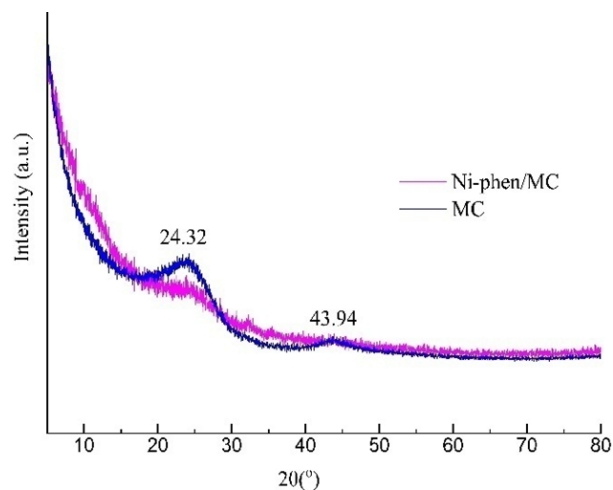
## 3. Results and Discussion

### 3.1 Synthesis and Characterization of Catalyst

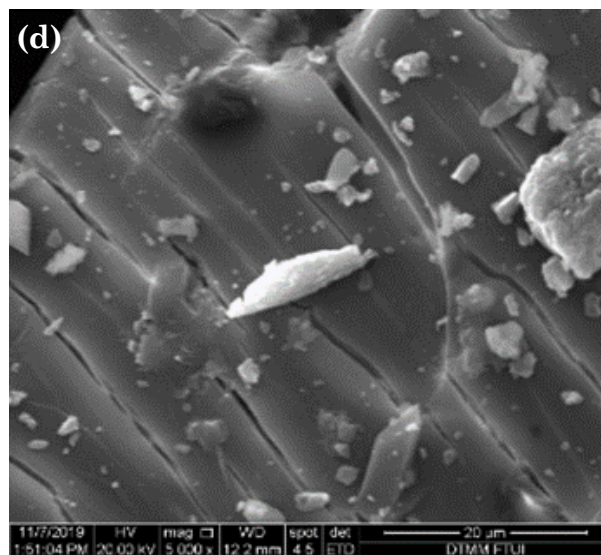
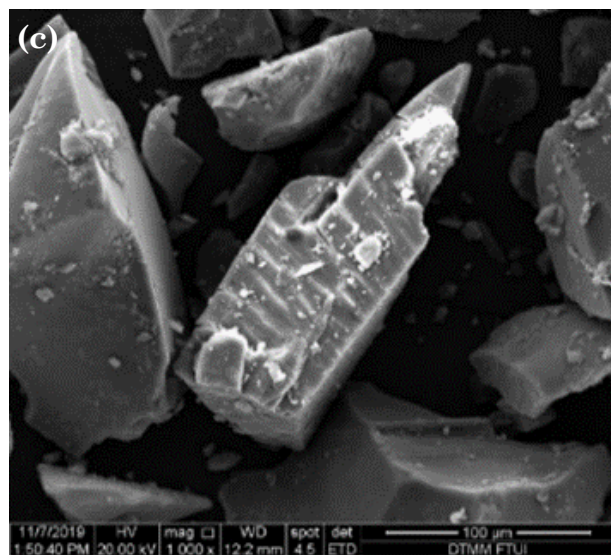
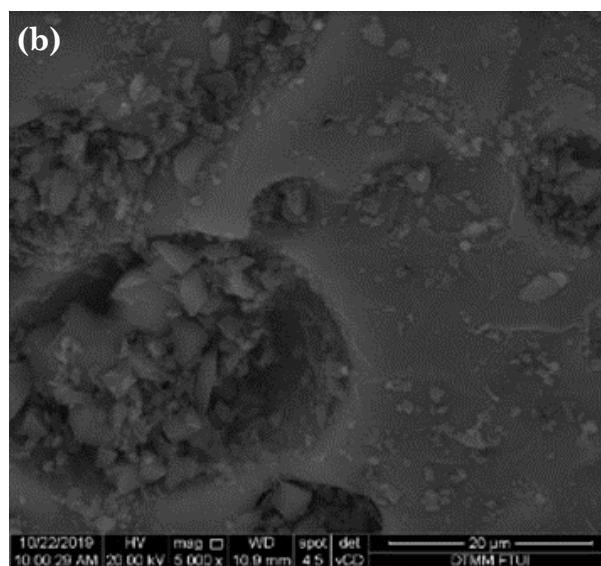
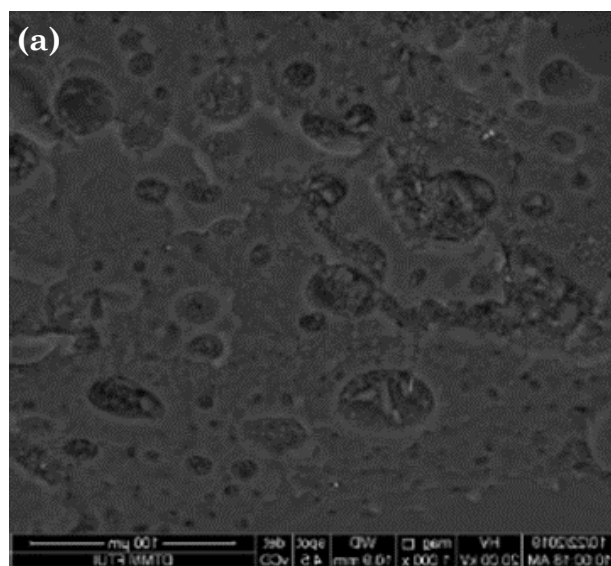
The synthesis of MC was performed using a soft template method with phloroglucinol and formaldehyde precursor as a carbon source, Pluronic F-127 as a template or surfactant, ethanol-water solution as medium for pluronic F-127 self-assembly and HCl 37% as catalyst for the polymerization reaction of phloroglucinol and formaldehyde. The hydrothermal treatment of the resulting monolith (polymerized form of carbon precursor) aims to the formation of meso-size pore and structure of mesoporous carbon. Whereas carbonization aims to polymer decomposition and to increase the surface area of mesoporous carbon [18]. The as-synthesized MC was then utilized as a solid support for Ni-phenanthroline complex.



**Figure 2.** The spectrum of (a) mesoporous carbon (MC), (b) activated carbon (AC), (c) 1,10-phenanthroline, and (d) Ni-phen/MC.



**Figure 3.** The XRD pattern of MC and Ni-phen/MC materials.



**Figure 4.** SEM image of (a) MC 1000X, (b) MC 5000X, (c) Ni-phen/MC 1000X, and (d) Ni-phen/MC 5000X magnification.



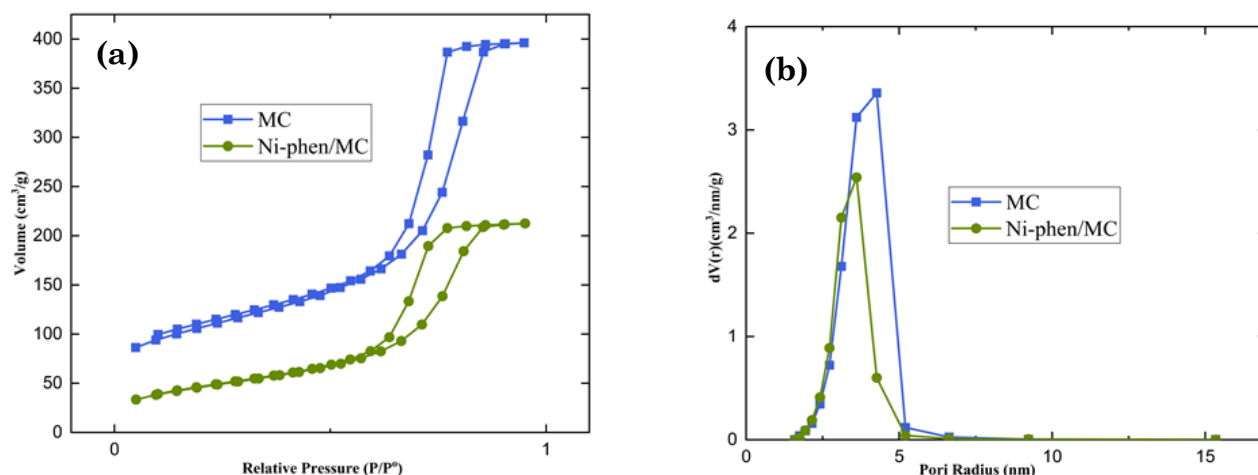
The 1,10-phenanthroline bidentate ligand forms a chelating effect by formation of coordination bonding to nickel ion [19]. Physical interaction could occur between mesoporous carbon with aromatic ring of phenanthroline ligands to give a heterogenized Ni-phen/MC catalyst.

IR spectra in Figure 1 show that the carbonization process proceeded well. This can be observed from removal of some functional groups such as O-H (stretching at  $3429\text{ cm}^{-1}$ ; bending at  $1619\text{ cm}^{-1}$ ) and C-H alkanes ( $2895\text{ cm}^{-1}$ ) which come from the phloroglucinol and formaldehyde precursors. We also compare the FTIR spectrum of MC with activated carbon (AC), phenanthroline ligand, and Ni-phen/MC (Figure 2). The spectrum of MC and AC showed similar pattern which indicate that both materials have almost no functional groups on their surface. In contrast to MC, the IR spectrum of phenanthroline consist of some peaks related to O-H stretching ( $3425\text{ cm}^{-1}$ ), C-H stretching ( $3050\text{ cm}^{-1}$ ), C-C stretching ( $1515\text{ cm}^{-1}$ ), C-N stretching ( $1383\text{ cm}^{-1}$ ), and C-H bending ( $846\text{ cm}^{-1}$ ) as shown in Figure 2c. Interestingly, Ni-phen/MC shows only one sharp peak at  $1383\text{ cm}^{-1}$  indicating the presence of C-N group [20]. These results suggest that the Ni-phen complex has been incorporated into the MC structure. The absence of the absorption peak of C-H

groups of phenanthroline indicates a strong interaction between aromatic ring of phenanthroline and mesoporous carbon.

The diffraction pattern of MC and Ni-phen/MC material are shown in Figure 3. Two peaks appear at  $2\theta$  of  $24.32^\circ$  and  $43.94^\circ$  which are the typical peaks of mesoporous carbon. These peaks have indices of 002 and 100 [21]. The diffractogram shows that the materials have an amorphous structure, and there was no significant structure difference between MC and Ni-phen/MC materials. Thus, the immobilization of Ni-phen complex does not alter the original structure of the mesoporous carbon.

The morphological and elemental analysis of MC and Ni-phen/MC were conducted using SEM-EDX characterization. Figure 4 shows surface morphology of MC and Ni-phen/MC with 1000 and 5000 magnification. The Ni-phen/MC has a smooth morphology compared with MC. In addition, there are some white particles of various sizes on the surface of the Ni-phen/MC indicating the presence of Ni-phen complex that has been attached to the surface of mesoporous carbon. Whereas Table 1 show the elemental composition on the surface of MC and Ni-phen/MC. According to the table, MC consist of 88.86% C and 11.14% O by weight. After the immobilization of Ni-phen complex,



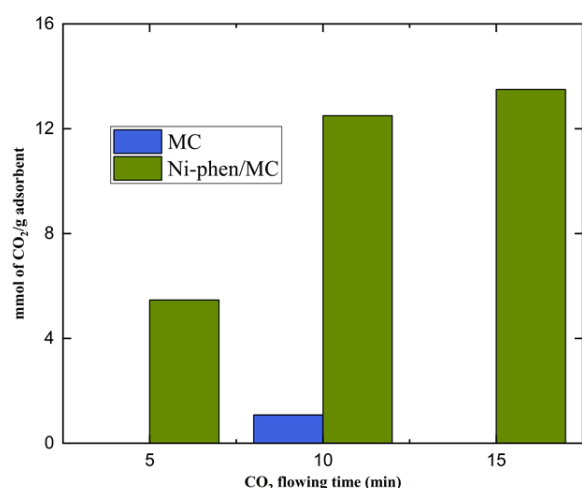
**Figure 5.** (a) adsorption-desorption isotherms curve of MC and Ni-phen/MC materials, (b) pore size distribution curve of MC and Ni-phen/MC.

**Table 1.** Elemental composition of MC and Ni-phen/MC by EDX.

Element	MC		Ni-phen/MC	
	Mass (%)	Atom (%)	Mass (%)	Atom (%)
C	88.86	91.4	88.06	92.14
O	11.14	8.6	8.67	6.79
Ni	-	-	3.27	1.06

Ni element was detected with a content of 3.27% which proves the immobilization of the complex on the surface of MC.

Nitrogen adsorption-desorption isotherm curve of MC and Ni-phen/MC are shown in Figure 5(a). The curves show that the two materials have similar type IV of hysteresis loops which is a typical curve for mesoporous material. However, as shown in Figure 5(b) there is a decrease in pore radius of the material after immobilization of the Ni complex, from 3.36 to 2.54 nm. This result indicates that some Ni complex enter the pores, thereby reducing the average pore diameter. In addition, there is also a decrease in the surface area of Ni-phen/MC which was most likely due to the partial filling of the carbon pores by the Ni complex. The surface properties of MC and Ni-phen/MC are summarized in Table 2.



**Figure 6.** The result of adsorption of CO<sub>2</sub>.

**Table 2.** Surface properties of MC and Ni-phen/MC.

Sample	$S_{\text{BET}}^a$ (m <sup>2</sup> /g)	$S_{\text{ext}}^b$ (m <sup>2</sup> /g)	$S_{\text{mic}}^b$ (m <sup>2</sup> /g)	$V_{\text{tot}}^c$ (cc/g)	$V_{\text{meso}}^d$ (cc/g)	$V_{\text{mic}}^c$ (cc/g)	Pore radius (nm)	Pore diameter (nm)
MC	364.873	274.6786	90.194	0.615	0.5664	0.045	3.3587	6.7174
Ni-phen/MC	165.59	156.2344	9.3556	2.1869	2.1838	9.3556	2.54	5.08

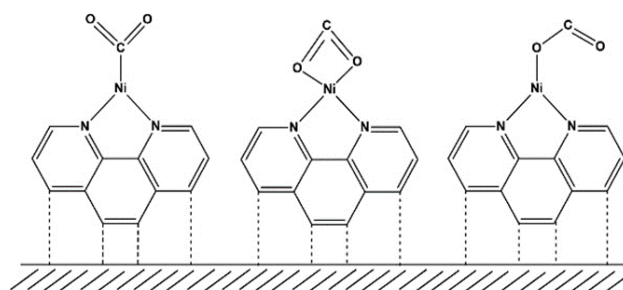
<sup>a</sup>calculated by BET method; <sup>b</sup>determined by t-plot; <sup>c</sup>calculated by BJH desorption method; <sup>d</sup>calculated by  $V_{\text{total}} - V_{\text{micro}}$

**Table 3.** Comparison of CO<sub>2</sub> adsorption capacities of some mesoporous carbon-based materials.

Material	CO <sub>2</sub> adsorption capacity (mmol/g)	Ref
TETA-modified MC	10.9	[20]
N-doped MC	5.7	[21]
NiNPs on N-doped MC	5.5	[21]
MDEA-modified MC	2.6	[22]
PANI/MC	5.6	[23]
Ni(phen)-modified MC	13.5	This work

### 3.2 Adsorption of Carbon Dioxide (CO<sub>2</sub>)

The adsorption performance of Ni-phen/MC towards CO<sub>2</sub> is presented in Figure 6. Based on the figure, the longer the flow of CO<sub>2</sub> to the sample, the greater the amount of CO<sub>2</sub> adsorbed. At a flow time of 5 minutes, 5.5 mmol of CO<sub>2</sub> was adsorbed per gram of adsorbent, and the values were increased to 12.5 and 13.5 mmol for flow times of 10 and 15 minutes, respectively. In addition, the CO<sub>2</sub> adsorption capacity of Ni-phen/MC is higher than that of the MC adsorbent, which is only 1.1 mmol of CO<sub>2</sub> at a flow time of 10 minutes (11 times higher). These results suggest that the presence of Ni-phen complex plays an important role in improving the adsorption capacity of mesoporous carbon. This can occur since the Ni species in the complex could bind to CO<sub>2</sub> molecule through several binding methods as shown in Figure 7. The results also show that the CO<sub>2</sub> adsorption capacity of Ni-phen/MC is higher than that of other mesoporous carbon-based materials such as amine-modified MC [20,22],



**Figure 7.** Proposed Ni-CO<sub>2</sub> interactions on Ni-phen/MC.

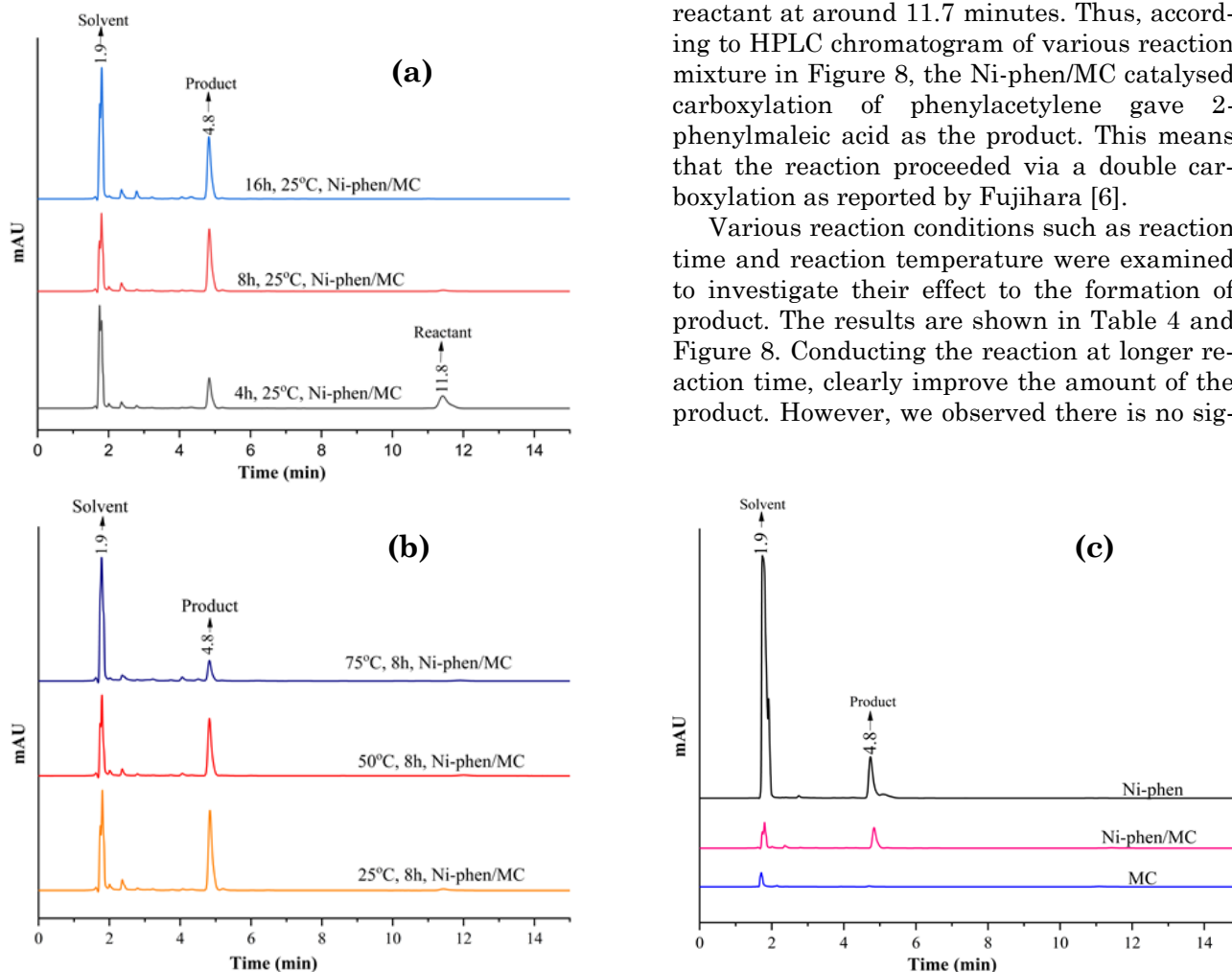
NiNPs-doped MC [21], and PANI/MC nanocomposite [23] (see Table 3 for details). This indicates the superiority of Ni-phen complex in binding to CO<sub>2</sub> compared to only amine functional group or nickel metal alone on MC.

### 3.3 Carboxylation Reaction of Phenylacetylene with CO<sub>2</sub>

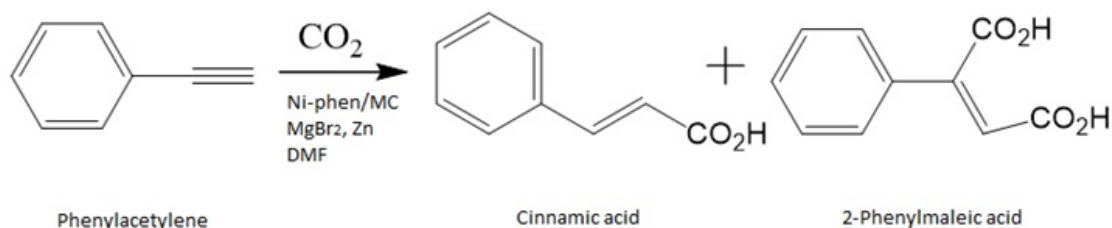
Based on previous studies [6,7] it is known that the homogeneous nickel-catalyzed carbox-

ylation of an alkyne could give two type of products, single- and double-carboxylation product. In the case of phenylacetylene as a substrate, the product could be cinnamic acid or 2-phenylmaleic acid, as shown in Scheme 1. Therefore, we investigate the reaction mixture by using the two product standards to determine the product of our Ni-phen/MC-catalysed carboxylation reaction. HPLC analysis of the standard shows that cinnamic acid appears at retention time of 6.1 min, 2-phenylmaleic acid at around 4.8 min, whereas phenylacetylene reactant at around 11.7 minutes. Thus, according to HPLC chromatogram of various reaction mixture in Figure 8, the Ni-phen/MC catalysed carboxylation of phenylacetylene gave 2-phenylmaleic acid as the product. This means that the reaction proceeded via a double carboxylation as reported by Fujihara [6].

Various reaction conditions such as reaction time and reaction temperature were examined to investigate their effect to the formation of product. The results are shown in Table 4 and Figure 8. Conducting the reaction at longer reaction time, clearly improve the amount of the product. However, we observed there is no sig-



**Figure 8.** HPLC chromatogram of reaction mixture of phenylacetylene carboxylation under various conditions: (a) variation of time, (b) variation of temperature, and (c) variation of catalyst type.



**Scheme 1.** Carboxylation of phenylacetylene catalysed by Ni-phen/MC in the presence of MgBr<sub>2</sub> as an additive, Zn powder as a reducing agent in DMF solvent under an atmospheric CO<sub>2</sub> pressure.

nificant difference for conducting the reaction for 8 and 16 h indicating that all reactants have been completely consumed after 8 h (Figure 8(a)). In contrast, temperature has the opposite effect to the reaction time, where an increase in temperature causes a decrease in the product formed. It can be understood that at higher temperatures, the solubility of CO<sub>2</sub> in the reaction medium (DMF) decreases, resulting in less products formed for the same reaction time (Figure 8(b)). We also compare the catalytic activity of Ni-phen/MC catalyst to the homogeneous Ni-phen catalyst and to MC alone as comparison. As the result, the heterogeneous Ni-phen/MC catalysts gave a product nearly half the amount of that formed from a homogeneous Ni-phen catalyst. This shows that the heterogeneous catalysts provide good prospects for further development in the future. The lower activity of the heterogeneous catalysts is understandable considering that the active site of the catalyst is less exposed than that in the homogeneous catalysts, in which the Ni-phen complex as an active species is free to move in the solvent medium and can interact with reactants on various sides. Meanwhile, when the reaction was carried out using MC in place of Ni-phen/MC, almost no product was formed. This result indicates that nickel is indeed the active species in the carboxylation reaction of phenylacetylene with CO<sub>2</sub>. Although MC has a surface area twice as large as Ni-phen/MC, the absence of an active catalyst causes the carboxylation reaction with CO<sub>2</sub> to not proceed.

#### 4. Conclusion

The heterogenization of nickel-phenanthroline complex was successfully conducted by immobilization on mesoporous carbon as a solid support as indicated by several characterization such as FTIR and SEM-EDX. The presence of the nickel complex on mesoporous carbon reduces the pore diameter and surface area of the support. However, the adsorption activity towards CO<sub>2</sub> increases due to the interaction between CO<sub>2</sub> with nickel-phenanthroline complex. Furthermore, the Ni-phen/MC catalyst show good performance in catalyzing the carboxylation reaction of phenylacetylene under an atmospheric CO<sub>2</sub> pressure.

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**Table 4.** HPLC chromatogram area of main product (retention time of 4.8 min).

Reaction conditions		Area (mAU)
Variation of time (h) <sup>a</sup>	4	17.9242
	8	36.9333
	16	36.1110
Variation of temperature (°C) <sup>b</sup>	25	36.9392
	50	26.0194
	75	9.5203
Variation of catalyst type <sup>c</sup>	Ni-phen	86.4172
	Ni-phen/MC	36.9041
	MC	1.7796

<sup>a</sup>reactions were conducted at 25 °C using Ni-phen/MC as a catalyst; <sup>b</sup>reactions were conducted for 8 h using Ni-phen/MC as a catalyst; <sup>c</sup>reactions were conducted at 25 °C for 8 h.



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