

Research Article

# Performance of Platinum Nanoparticles / Multiwalled Carbon Nanotubes / Bacterial Cellulose Composite as Anode Catalyst for Proton Exchange Membrane Fuel Cells

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## Abstract

Highly dispersed platinum (Pt) nanoparticles / multiwalled carbon nanotubes (MWCNTs) on bacterial cellulose (BC) as anode catalysts for proton exchange membrane fuel cells (PEMFC) were prepared with various precursors and their electro-catalytic activities towards hydrogen oxidation at 70 °C under non-humidified conditions. The composite was prepared by deposition of Pt nanoparticles and MWCNTs on BC gel by impregnation method using a water solution of metal precursors and MWCNTs followed by reducing reaction using a hydrogen gas. The composite was characterized by using TEM (transmission electron microscopy), EDS (energy dispersive spectroscopy), and XRD (X-ray diffractometry) techniques. TEM images and XRD patterns both lead to the observation of spherical metallic Pt nanoparticles with mean diameter of 3-11 nm well impregnated into the BC fibrils. Preliminary tests on a single cell indicate that renewable BC is a good prospect to be explored as a membrane in fuel cell field. Copyright © 2017 BCREC Group. All rights reserved

**Keywords:** Anode catalyst; Platinum nanoparticles; Multiwalled carbon nanotubes; Bacterial cellulose; Proton exchange membrane fuel cell

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## 1. Introduction

Proton exchange membrane fuel cells (PEMFC) are costly electrochemical energy conversion devices, but they are receiving

increasing attention due to their environmentally friendly characteristics [1-2]. The PEMFC produces electricity as long as the fuel (usually hydrogen) and oxidant (usually oxygen) are supplied continuously to the respective anode and cathode. Pure water is the only by-product of PEMFC. The efficiency of energy conversion in

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PEMFC is dependent on the catalytic activities of the catalysts used in the cathode and anode of membrane electrode assemblies (MEAs). MEAs are considered the heart of PEMFC without which they cannot produce electricity. A typical method of making the MEA is hot pressing catalyst layers onto polymer electrolyte membranes (PEMs) [3-4]. The catalyst layers are prepared separately by painting, spraying or printing catalyst inks containing catalyst particles and polymer electrolyte suspension on the surface of carbon electrodes (gas diffusion layers, GDL). GDL with catalyst particles are used for both anode and cathode, and with either carbon or metal interconnects. The most commonly used catalyst in PEMFC are platinum (Pt)-based metals supported on high surface area carbon [5-6]

Yang *et al.* [7] have developed alternative new hydrocarbon-based polymer membranes that are bacterial cellulose (BC). The electrode used was BC coated Pt catalyst and carbon by way of brushing, and Pt catalyst performance has been analyzed with the PEMFC. Meanwhile, Aritonang *et al.* [8] have been coating BC by immersion into a solution of Pt precursors and carbon powder. The results showed that the Pt nanoparticles and carbon trapped in pores and spread evenly on the fibers of BC. The immersion method is more effective because it does not require much time, but the performance of Pt and carbon powder on BC membrane as the catalyst has not been done.

This paper reported that highly dispersed Pt nanoparticles are impregnation deposited by reduction method on the surface of BC (followed by insertion of MWCNTs on the BC surface). In addition, the electro catalytic activity of Pt/MWCNTs/BC anode for hydrogen oxidation is also investigated. Therefore, the purpose of this study was to analyze the performance of Pt nanoparticles on a composite Pt/MWCNT/BC as a catalyst in hydrogen fuel cells.

## 2. Materials and Methods

### 2.1. Materials

Platinum tetrachloride ( $\text{PtCl}_4$ ), potassium tetrachloroplatinate (II) ( $\text{K}_2\text{PtCl}_4$ ), and 5wt% Nafion® solution were obtained from Sigma-Aldrich (99,9%), while ammonium sulfate  $[(\text{NH}_4)_2\text{SO}_4]$ , glacial acetic acid ( $\text{CH}_3\text{COOH}$ ), hydrochloric acid (HCl), sodium hydroxide (NaOH), ethanol ( $\text{CH}_3\text{CH}_2\text{OH}$ ), cetyltrimethylammonium bromide (CTAB), Nafion® 117 (Dupont), 5% hydrogen peroxide ( $\text{H}_2\text{O}_2$ ), were obtained from Merck. Carbon electrode

(cathode catalyst as 20%Pt/C) from Johnson Matthey, MWCNTs with outer diameters of 8-15 nm, length  $\sim 50\mu\text{m}$  and purity of  $>95\%$  was purchased from He Ji Limited Company, Hongkong. Hydrogen gas (ultra highly pure) was obtained from a local supplier. Coconut water, sucrose (food-grade white sugar) and *Acetobacter xylinum* were obtained from a local traditional market. All chemicals were used without further purification.

### 2.2. Preparation of Pt nanoparticles MWCNTs / BC

Preparation of BC was carried out as described previously by Radiman & Yuliani [9]. To obtain dry BC membranes, the BC gel was first cut to a size of 4 cm  $\times$  4 cm, then pressed to remove water and finally air dried at room temperature for 6 days. MWCNTs were dispersed in deionized water with a cationic surfactant, cetyltrimethylammoniumbromide (0.1 wt %). Ultrasound was applied to obtain a homogeneous dispersion using an ultrasonic generator (Branson® 2510E-DTH) for 2 h at 25 °C.

The pressed BC membrane was soaked in aqueous a solution containing 20 mM  $\text{PtCl}_4$  and sonicated at room temperature for 2 h. The BC gel was removed, rinsed with deionized water and soaked again in a MWCNTs solution and sonicated at room temperature for another 2 h. The  $[\text{PtCl}_4]/\text{MWCNTs}/\text{BC}$  gel was removed, rinsed with deionized water and soaked in deionized water and then pressed to remove water and to obtain the dry composite membrane. The membrane was then reduced with hydrogen gas at an applied constant pressure of 0.5 psi and a stirring speed of 500 rpm at room temperature for 1 h. The Pt-MWCNTs-BC gel was removed from the solution and dried, as in the above procedure, and produced a dry composite that is denoted by  $\text{Pt}_{\text{PtCl}_4}\text{-MWCNTs-BC}$ . The same procedure was carried out using  $\text{K}_2\text{PtCl}_4$  and  $\text{H}_2\text{PtCl}_6$  precursor and composites derived were designated as  $\text{Pt}_{\text{K}_2\text{PtCl}_4}/\text{MWCNTs}/\text{BC}$  and  $\text{Pt}_{\text{H}_2\text{PtCl}_6}/\text{MWCNTs}/\text{BC}$ .

### 2.3. Physical characterization

X-ray diffraction spectra were recorded using PW1835 Philips diffractometer (Japan) at 40 kV and 30 mA. The  $2\theta$  angular regions between 5 and 90° were explored at a scan rate of 0.020°/sec. Transmission electron microscopy (TEM) images were recorded using a JEOL JEM-1400(Japan) operating at 120V and an acceleration voltage of 15 kV. For TEM measure-

ments, composites were heated at 600°C degrees to remove BC. The residue formed by Pt nanoparticles was suspended in ethanol. A drop of the suspension was deposited on the copper grid. The information was added in the text. The particle sizes of the Pt nanoparticles were measured using Image J software. At least 200 particles of each sample from different TEM images were analyzed. The histogram of the size distribution was established by Origin software.

## 2.4. Single cell tests

Single-cell PEMFC performance of the composites was evaluated by a fuel cell test station. The anode and cathode material were composite and carbon paper that was coated with 20% Pt/C, respectively. The composites were dripped with 1 drop of 5 wt% Nafion® solution and dried at room temperature. Nafion® 117 membrane was used as a polymer electrolyte membrane. Nafion® 117 membrane was preconditioned prior to fabrication of membrane electrode assembly (MEA) to remove impurities. First, Nafion® 117 membrane was boiled in 5% hydrogen peroxide at 80 °C. Then, it was boiled in 0.5 M H<sub>2</sub>SO<sub>4</sub> at 80 °C to let protons change to a form of hydrogen ion. Finally, the treated membranes were stored in aquadest prior to use [10].

The MEA obtained was mounted in a single cell with stainless steel end plates and graphite collector plates, which was designed with parallel ribbed channels for gas manifold. The MEA was fabricated by sandwiching the Nafion® 117 membrane between the anode and cathode by hot pressing at 90 °C and 0.1 ton for 180 s. The active cell area and thickness were 1 cm<sup>2</sup> (1×1 cm<sup>2</sup>) and 0.28 mm, respectively. The fuel cell testing is carried out at 1 atmospheric pressure and operating temperature of 70 °C with pure hydrogen and oxygen gas reactants.

## 3. Results and Discussion

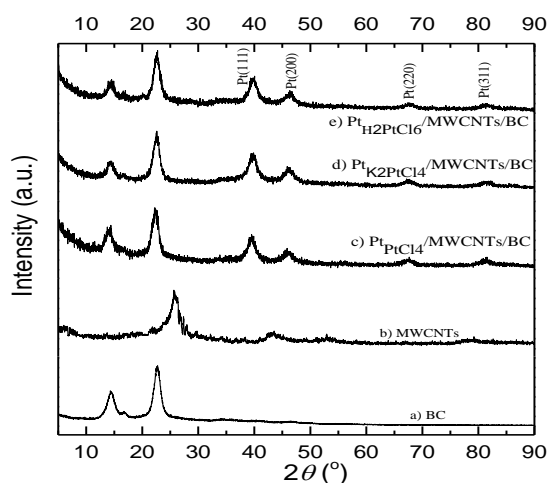
### 3.1. XRD, TEM, and EDX analysis of the Pt/MWCNTs/BC membranes

Figure 1 shows the powder X-ray diffraction patterns of the Pt/MWCNTs/BC membranes. All the composites exhibited four characteristic diffraction peaks of Pt at 2θ values around 40°, 46°, 68°, and 81° corresponding to the (111), (200), (220), and (311) planes, respectively. These peaks indicated that Pt is present in the face-centered cubic (fcc) structure (nearly identical to the standard values ICSD number 76951). The broad diffraction peaks of Pt in the

composites are indicative of the nanosized Pt.

The average crystallite size of Pt supported on BC membrane is calculated from line broadening of the (200) diffraction peak (Gaussian-Lorentzian peak) according to Scherrer's equation  $L = (0.9\lambda)/(B \cos \theta)$ , where  $\lambda$  is the wavelength of the X-ray (1.5406 Å),  $\theta$  is the angle at the position of the peak maximum, and  $B$  is the width (in radians) of the diffraction peak at half height [11]. The measured Pt crystallite size in the Pt<sub>PtCl<sub>4</sub></sub>/MWCNTs/BC, Pt<sub>K<sub>2</sub>PtCl<sub>4</sub></sub>/MWCNTs/BC, and Pt<sub>H<sub>2</sub>PtCl<sub>6</sub></sub>/MWCNTs/BC composite is 3.4, 11.3, and 6.9 nm, respectively. Besides diffraction peaks of Pt, there are also three characteristic diffraction peaks of BC around 14°, 17°, and 22°. BC peaks appeared on the Pt/MWCNTs/BC composite and similar to BC membrane itself. Meanwhile, the peak of MWCNTs did not appear on the third composites because it has been covered by Pt particles.

Figure 2 shows the TEM images of the Pt nanoparticles. The size and size distribution of the Pt nanoparticles formed on the different precursors were analyzed by using TEM, and the histogram based on the TEM images illustrated their average size and size distribution. As seen in the figures, the Pt nanoparticles formed in every test composites exhibited a small size and a narrow size distribution. However, few Pt agglomerations are observed from K<sub>2</sub>PtCl<sub>4</sub> and H<sub>2</sub>PtCl<sub>6</sub> precursor. The data on particle size distribution revealed the presence of Pt nanoparticles in size range of 2-38 nm, with an average size of 3, 11, and 6 nm from the PtCl<sub>4</sub>, K<sub>2</sub>PtCl<sub>4</sub>, and H<sub>2</sub>PtCl<sub>6</sub> precursor, respectively. The data show that the size of Pt



**Figure 1.** XRD patterns of a) BC, b) MWCNTs, c) Pt<sub>PtCl<sub>4</sub></sub>/MWCNTs/BC, d) Pt<sub>K<sub>2</sub>PtCl<sub>4</sub></sub>/MWCNTs/BC, and e) Pt<sub>H<sub>2</sub>PtCl<sub>6</sub></sub>/MWCNTs/BC composite

nanoparticle from PtCl<sub>4</sub> precursor is relatively smaller than other precursors with narrower particle size distribution (σ).

The particle sizes measured from TEM images are almost comparable with those of the crystallite sizes determined from XRD. It indicates the existence of Pt particles as single crystallites on BC membrane support. The average sizes of the Pt nanoparticles of all the precursors calculated from the XRD peak widths agreed well with the TEM results. The morphological data of all the Pt nanoparticles are presented in Table 1. The surface areas of these Pt catalysts are calculated from the mean diameter of the particles obtained from the

TEM images by using the equation:

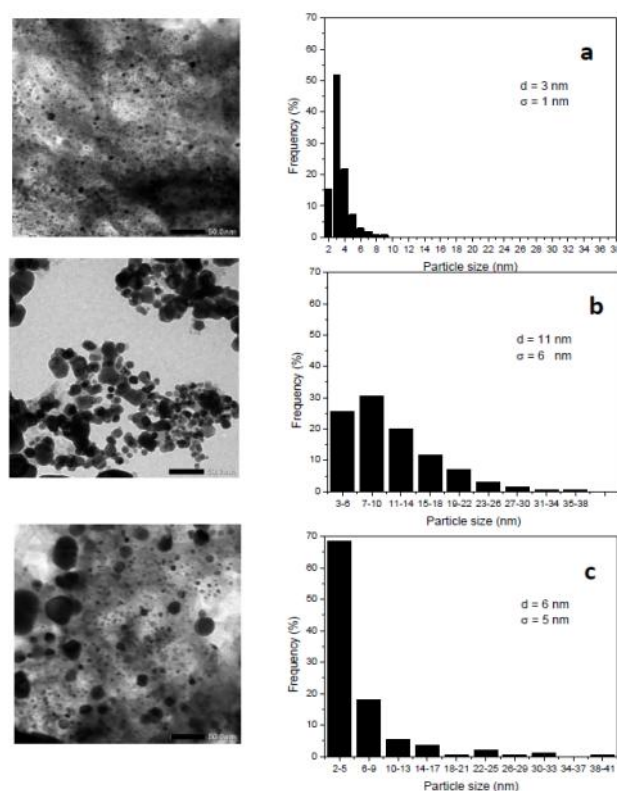
$$S = 6000/d\rho \quad (1)$$

where ρ is the Pt density (21.45 g/cm<sup>3</sup>), d is the particle size (in nm) [12]. Among all the Pt nanoparticles, the surface area is found to be the largest for the Pt from PtCl<sub>4</sub> precursor because of its smaller particle size with good dispersion on the BC membrane.

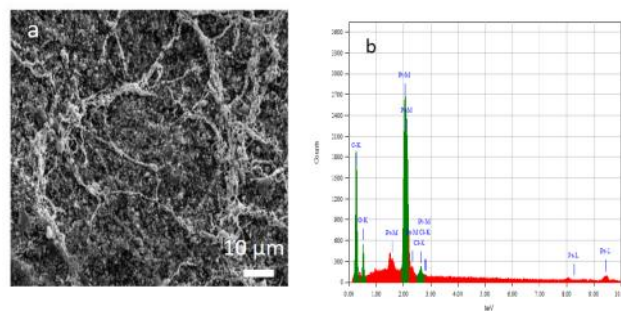
By EDS investigation, the Pt content was tested to the composite and composition of Pt are presented in Table 1. The data show that the content of the Pt particles is derived from PtCl<sub>4</sub> precursor relatively more than those from other precursors. The measurement of Pt<sub>PtCl<sub>4</sub></sub>/MWCNTs/BC composite was taken as an example and is demonstrated in Figure 3.

### 3.2. Fuel cell performance

Figure 4 compares the performance of the PEMFC at 70 °C using Pt catalyst on the Pt/MWCNTs/BC composite as the anode under the same testing conditions. The results showed that Pt nanoparticles contained in the composite anode of Pt/ MWCNTs/BC could serve as a catalyst for the oxidation of hydrogen. This can be seen in the performance profile of Pt on PEMFC for each electrode, which is expressed in a curve polarization current (I) of the potential (V) and power (W), which is



**Figure 2.** TEM images and particle size distribution histograms of Pt nanoparticles formed in BC membranes prepared from PtCl<sub>4</sub> (a), K<sub>2</sub>PtCl<sub>4</sub> (b) and H<sub>2</sub>PtCl<sub>6</sub> (c) as the precursor source



**Figure 3.** Typical SEM image (a) and the corresponding EDS pattern (b) of the Pt<sub>PtCl<sub>4</sub></sub>/MWCNTs/BC membrane

**Table 1.** EDX composition and comparison of morphological data of the Pt nanoparticles prepared at different precursors on composites

Composites	EDX composition of Pt	Particle size from TEM (nm)	Particle size from XRD (nm)	Surface Area (m <sup>2</sup> g <sup>-1</sup> )
Pt <sub>PtCl<sub>4</sub></sub> /MWCNTs/BC	51.43	3	3.4	93.24
Pt <sub>K<sub>2</sub>PtCl<sub>4</sub></sub> /MWCNTs/BC	29.77	11	8.3	25.43
Pt <sub>H<sub>2</sub>PtCl<sub>6</sub></sub> /MWCNTs/BC	47.01	6	5.2	46.62

carried out at a temperature of 70 °C.

The performance of anode shows that maximum power density for three composites (electrode) are different. At 0.07 V, Pt catalyst on the Pt<sub>PtCl4</sub>/MWCNTs/BC composite yielded a current density and power density are 1.94 mA.cm<sup>-2</sup> and 0.13 mW.cm<sup>-2</sup>, respectively. Meanwhile, other composite showed that a much lower value, as shown in Table 2.

PEMFC performance using composite anodes showed patterns similar profiles for all of the electrodes, but it has optimum peak power density of different. When using the Pt<sub>(K2PtCl4)</sub>/MWCNTs/BC electrode, the performance of Pt on PEMFC produces optimum peak power density of 0.02 mW/cm<sup>2</sup> at current densities of 0.60 mA/cm<sup>2</sup>, while using Pt<sub>(H2PtCl6)</sub>/MWCNTs/BC electrode, the optimum power density of 0.03 mW/cm<sup>2</sup> at current density of 0.30 mA/cm<sup>2</sup> and using Pt<sub>(PtCl4)</sub>/MWCNTs/BC electrode, optimum power density of 0.11 mW/cm<sup>2</sup> at current densities of

2.10 mA/cm<sup>2</sup>.

Optimum power density generated by the Pt<sub>(PtCl4)</sub>/MWCNTs/BC electrode larger than the other electrode. This is due to the high content of Pt nanoparticles contained in the electrode. In addition, the size distribution of Pt nanoparticles smaller than PtCl<sub>4</sub> precursor sources, have an impact on current density and optimum power greater than the Pt nanoparticles from other Pt precursor sources. This is because the particle size distribution of Pt affects the course of the oxidation reaction of hydrogen [13].

This performance difference in the activation region can be attributed mainly to the difference in the Pt particle size between on the Pt<sub>PtCl4</sub>/MWCNTs/BC (3 nm), Pt<sub>K2PtCl4</sub>/MWCNTs/BC (11 nm), and Pt<sub>H2PtCl6</sub>/MWCNTs/BC (6 nm) composite. In addition, the content of Pt on the composite can also affect the cell performance [14]. Furthermore, in the ohmic polarization region, the cell performance using Pt<sub>K2PtCl4</sub>/MWCNTs/BC and Pt<sub>H2PtCl6</sub>/MWCNTs/BC composites are also lower than that using the Pt<sub>PtCl4</sub>/MWCNTs/BC composite.

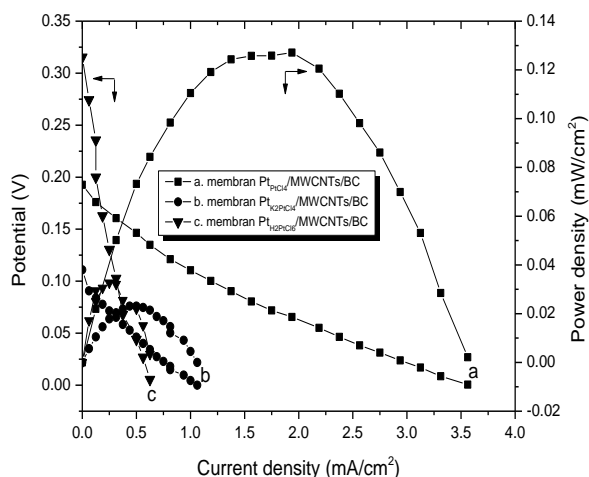


Figure 4. Comparison of single cell polarization curves for the PEMFC in presence of Pt<sub>PtCl4</sub>/MWCNTs/BC, Pt<sub>(K2PtCl4)</sub>/MWCNTs/BC, Pt<sub>(H2PtCl6)</sub>/MWCNTs/BC anode catalysts; cathode: Pt/C (20 wt.%, Johnson Matthey Corp.); electrolyte membrane: Nafion-117®(DuPont) membranes; operation temperature: 70 °C

#### 4. Conclusion

The performance of a PEMFC is studied with Pt/MWCNTs/BC composite and Pt black catalysts as anode and cathode catalysts, respectively. The effect of Pt size as a catalyst on composite is studied. The Pt<sub>PtCl4</sub>/MWCNTs/BC composite is seen to give the best performance for a PEMFC when used as an anode catalyst because the size of Pt particle, size distribution and Pt content on composite are smaller, narrow size and more content, respectively than other precursors.

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Table 2. Comparison of potential, current density, and optimum power density using different composite anode

Pt <sub>PtCl4</sub> /MWCNTs/BC			Pt <sub>K2PtCl4</sub> /MWCNTs/BC			Pt <sub>H2PtCl6</sub> /MWCNTs/BC		
Poten- tial (V)	Current density (mA/cm <sup>2</sup> )	Power density (mW/cm <sup>2</sup> )	Poten- tial (V)	Current density (mA/cm <sup>2</sup> )	Power density (mW/cm <sup>2</sup> )	Poten- tial (V)	Current density (mA/cm <sup>2</sup> )	Power density (mW/cm <sup>2</sup> )
0.07	1.94	0.13	0.05	0.60	0.02	0.07	0.30	0.03

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