



Research Article

Electrochemical Generation of Hydrogen and Methanol using ITO Sheet Decorated with Modified-Titania as Electrode

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Abstract

Current issues of global warming and environmental pollution due to extensive use of fossil fuels has been reached to an alarming position. Being CO₂ as main byproduct of fossil fuel consumption and water as abundantly available on earth surface has great potential to replace fossil fuels as energy source. Herein, electrocatalytic CO₂ reduction with water for methanol and hydrogen gas (H₂) production over ITO sheet decorated with modified-Titanium nanorods (TiO₂ NR), has been investigated. The performance comparison of electrocatalytic activity of hydrothermally modified-titania with commercial TiO₂ microparticles (MP) were further investigated. Electrochemical reactor containing KHCO₃ aqueous solution with CO₂ as an electrolyte and modified TiO₂ nanorods (NR) as working electrodes offer an eco-friendly system to produce clean and sustainable energy system. The typical rates of product, *i.e.* methanol and H₂ generation from the ITO sheet decorated with modified TiO₂ NR layer recorded higher than those for the ITO sheet with commercial TiO₂ microparticle. At 2.0V applied potential vs Ag/AgCl as reference electrode, the modified TiO₂ NR electrocatalyst yielded methanol at a rate of 3.32 $\mu\text{mol.cm}^{-2}.\text{L}^{-1}$ and H₂ at a rate of 6 $\mu\text{mol.cm}^{-2}.\text{L}^{-1}$ which was higher than that of commercial TiO₂ MP electrocatalyst (methanol = 1.5 $\mu\text{mol.cm}^{-2}.\text{L}^{-1}$ and H₂ = 3.7 $\mu\text{mol.cm}^{-2}.\text{L}^{-1}$). The enhancement in product yields of methanol and H₂ was mainly due to the notable improvements and modification in texture of TiO₂ working electrode interface. Hence, it is concluded that the modified TiO₂ NR can be considered as a competent candidate for sustainable energy conversion applications.

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Keywords: CO₂ electroreduction; water electrocatalysis; methanol; hydrogen; TiO₂ nanorods

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1. Introduction

Currently, the earth's main energy sources are mostly depending on non-renewable fossil fuels such as petroleum oils, coal and natural

gas [1–2]. These sources of energy are limited in nature, and their utilization and consumption process cause environmental pollution due to the emission of greenhouse gases (CO₂) and air pollution (SO_x and NO_x), all of these problems lead to global warming and serious climatic changes [3–4]. A cleaner production of hydrogen (H₂) has a great potential to substitute fossil fuel utilization due to its immense advantages, such as higher energy density and zero carbon

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footprint up on use. Presently, most of the H₂ production is commercially done by steam reforming of natural gas, which causes CO₂ emissions [5]. Electrochemical (EC) process can be used to produce H₂ via electrocatalysis of water under low electrical bias. The CO₂ produced as byproduct of steam reforming of natural gas and utilization of other fossil fuels can also be converted back to methanol using EC process. The electrocatalytic efficiency of CO₂ reduction and direct water electrocatalysis depends on the working electrode or semiconductor used as electrocatalyst.

In recent years, numerous semiconductor materials, such as: SnO₂, InP, CdS, g-C₃N₄, Bi₂WO₆, Cu₂O, InSe₂, BiVO₄, PbO₂, rGO, CeO₂ and TiO₂ [6–12], have been investigated as electrocatalysts in EC system for CO₂ and reduction H₂ evolution reaction. However, TiO₂ has been considered as a standard benchmark for researchers after the pioneering research work conducted by Fujishima and Honda for electrocatalytic process [13,14]. High demand for TiO₂ as electrocatalyst is due to high stability in a corrosive environment, facile in preparation and structure modification, abundant availability, economical in cost and ecofriendly [15,16]. In EC applications, TiO₂ has been extensively investigated for both CO₂ reduction and water oxidation for methanol and H₂ evolution reactions [9,17,18]. Particularly, TiO₂ is considered as one of the promising electrocatalyst and semiconductor for EC processes because of its easy availability, cheap, negative flat band potential, unique electronic configuration, stable towards corrosive chemicals and ecofriendly. However, commercially available TiO₂ microparticle suffers from rapid recombination of charge, lower product selectivity, larger bandgap (~3.2 eV), and less catalytic efficiency [19]. This is due to the lower surface area and fast electrons (e⁻) and holes (h⁺) recombination rates which effects the efficiency of electrocatalytic activity methanol and H₂ production [20]. Both properties of TiO₂ affect the efficiency of catalytic activity in methanol and H₂ production [21].

The efficiency of TiO₂ can be improved by surface modification and changing the structure of TiO₂ crystals. TiO₂ exists in various structural phases such as brookite, rutile and anatase [22]. The anatase phase of TiO₂ is considered most efficient in electrocatalytic processes as compared to brookite and rutile phase. Moreover, the catalytic efficiency highly relies on the crystal structures of TiO₂ which exist in various forms, such as: microparticles,

nanoparticles, and nanorods. High catalytic activity could be obtained with nanorods structures due to higher active sites or surface area compared to the microparticles and nanoparticles [23]. The structural morphologies can be controlled based on the synthesize method of TiO₂. The problem of charge recombination and surface area can be addressed by changing and modification of surface morphology of TiO₂ for better charge transfer and enhanced surface area [24,25]. Based on these assumptions and viewpoints, herein, we aimed to synthesize simple and uniquely modified TiO₂ nanorods electrocatalyst for efficient CO₂ reduction and direct electrocatalysis of water to produce methanol and H₂.

In this study, we synthesis the TiO₂ nanorods via hydrothermal method using sodium hydroxide as alkaline agent. The as prepared TiO₂ nanorod (NR) sample was used to fabricate electrode for electrocatalytic CO₂ reduction into methanol and H₂ production by using catalyst ink method. Commercial TiO₂ microparticles (MP) were also used in the electrode fabrication for comparison purpose. The synthesized TiO₂ NR and commercial TiO₂ MP were characterized to analyze the structural phase and surface morphology by using X-ray Diffraction (XRD), Brunauer-Emmett-Teller (BET), Field Emission Scanning Electron Microscope (FESEM), and High-resolution transmission electron microscopy (HR-TEM) techniques. Both TiO₂ NR and commercial TiO₂ MP electrodes were subjected to electrocatalytic CO₂ reduction for the electrocatalytic performance evaluation on the basis of methanol and H₂ production.

2. Materials and Methods

2.1 Materials

Titanium(IV) oxide (TiO₂), anatase (99.9%), Sodium hydroxide (NaOH) (97.0%) and Dimethylsulfoxide (DMSO) (99.5%) were analytical grade reagents and used without further purification. Indium tin oxide coated glass slide (ITO), surface resistivity 15-25 Ω/sq, Platinum (Pt) wire (purity = 99.9%), Ag/AgCl (3.5 M KCl) reference electrode and all other chemical were purchased from Sigma-Aldrich Sdn Bhd, Malaysia. Carbon dioxide (CO₂) gas (purity = 99.9%), Hydrogen (H₂) gas (purity = 99.9%) and all other gases required for gas chromatograph (GC) system were acquired from Mega Mount Industrial Gases Sdn. Bhd., Malaysia. Deionized water was used as solvent for all aqueous solutions.

2.2 Synthesis of Electrocatalyst

TiO₂ NR synthesized by using hydrothermal method, reported elsewhere [26]. In this method 1.5 g of TiO₂ (anatase) powder was added to 70 mL of NaOH (10 M) aqueous solution. After stirring for 1 h, the solution was transferred to a 100 mL autoclave and heated at 200 °C for 24 h. The precipitate was centrifuged and washed with deionized water and ethanol several times until the pH value reached ~7. The wet product was kept in an oven for drying at 100 °C for 12 h. The obtained sample was crushed and calcined in a furnace at 500 °C for 5 h. The synthesized sample is denoted by TiO₂ NR afterwards.

2.3 Synthesis of Electrode

Modified TiO₂ NR electrode was fabricated on ITO slide by using catalyst ink method. For this purpose, 0.1 g of TiO₂ NR was mixed in 10 μ L DMSO and sonicated for 6 h to synthesis evenly dispersed and viscous catalyst ink. After preparation of catalyst ink, the ITO slide was carefully covered with catalyst ink by drop casting method. The ITO slide covered with catalyst ink was then transferred to oven for drying at 100 °C for 6 h.

2.4 Catalyst Characterizations

The structure and degree of crystallinity were carried out using XRD technique. The XRD patterns were obtained by the D5000 Siemens instrument using Cu-K α radiation (40 keV, 40 mA). The patterns were evaluated at a scanning rate of 1.2 °.min⁻¹ and a scanning range of 10–90° of 2 θ . The diffractometer is armed with a Ni-filtered Cu K α radiation source ($\lambda = 1.54056 \text{ \AA}$). The X-ray source was operated at 40 kV and 200 mA. The phase identification of the as-prepared sample was analyzed by comparison to Joint Committee on Powder Diffraction Standards (JCPDS). The morphology of the electrodes and catalyst powder was analyzed by field emission scanning electron microscopy (FESEM) by using Hitachi SU8020. The high-resolution transmission electron microscope (HR-TEM) images of the as-prepared electrocatalyst samples was obtained from the JEOL JEM-ARM 200F HR-TEM transmission electron microscope. Electrochemical characterizations such as cyclic voltammetry (CV) was performed by using an electrochemical workstation (Keithley-2450-EC, Tektronix, USA). In a typical three-electrode system with 0.1 M KHCO₃ as electrolyte in a homemade EC microreactor (100 cm³)

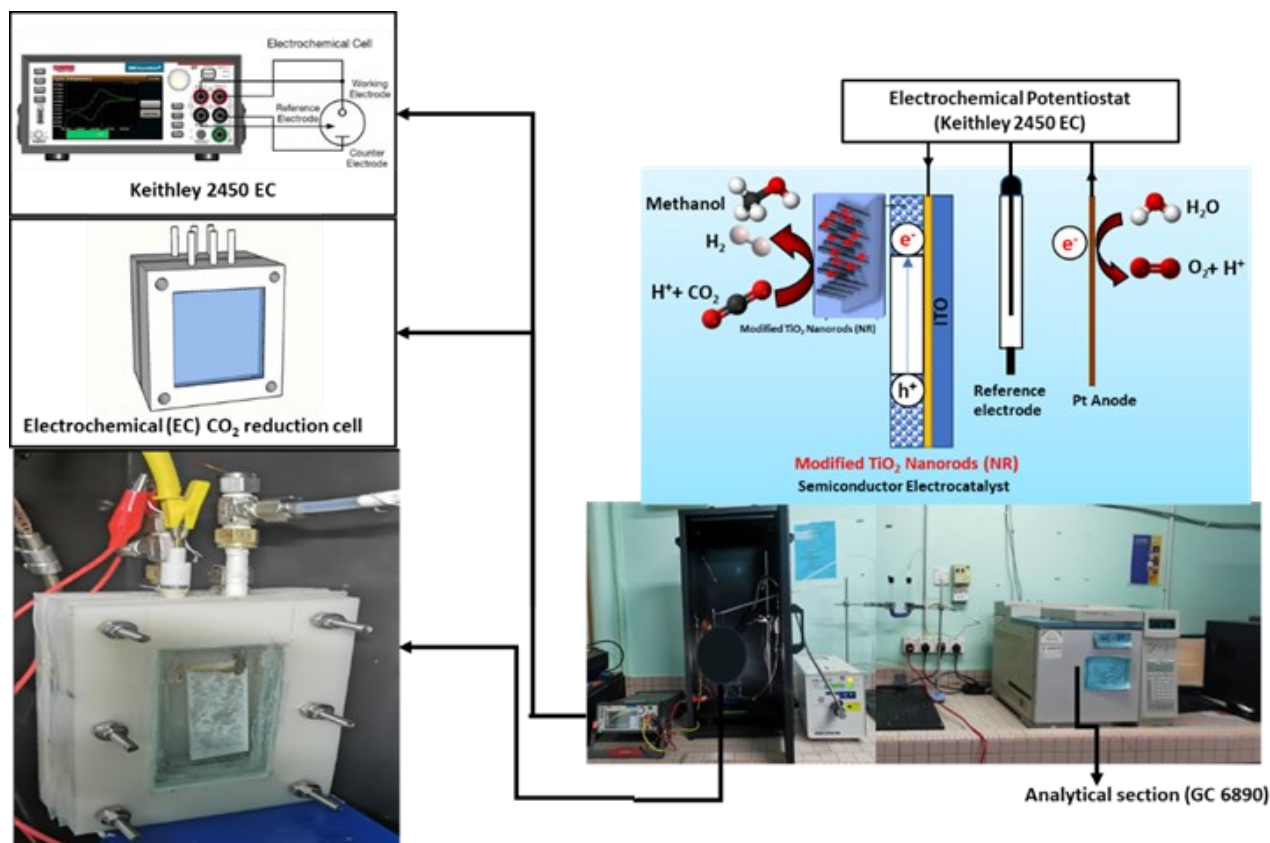


Figure 1. Electrochemical (EC) experimental setup with schematic diagram of the process.

with continuous flow/bubbling of CO₂ at 20 m/min. The prepared electrocatalyst samples, platinum plate and standard Ag/AgCl electrode were used as working, counter and reference electrode, respectively.

2.5 Experimental Setup and Reactor Configuration

The schematic of experimental setup for the homemade electrocatalytic (EC) reactor system is presented in Figure 1. The KHCO₃ (0.1M) as

electrolyte for the EC reaction system is fed into the EC reactor cell. Then, the CO₂ is introduced into EC reactor cell by a digital mass flow controller (Alicat Scientific Mc-1Slpm-D (CO₂)) at a flow rate of 20 mL/min. The potential difference across EC reactor cell was applied by an electrochemical workstation (Keithley-2450-EC, Tektronix, USA) in a typical three-electrode system. The prepared electrocatalyst samples coated on ITO slide, platinum plate and standard Ag/AgCl electrode is used as working, counter and a reference electrode, respectively. To analyze the electrocatalysis for H₂ production and CO₂ reduction for methanol production under light irradiation, a solar simulator model number LAX-C100, Asahi Spectra was used as light source. The gas products were analyzed through an online gas chromatograph (GC) system (model No: Agilent 6890N) connected with a thermal conductivity detector (TCD) and Carbon-PLOT capillary column (0.53 mm × 30 m). The temperature of the GC system column was set at 200 °C. The liquid product was analyzed through an offline gas chromatograph (GC) system (model No: Agilent 7820N) connected with a Flame-ionization detection (FID) and a DB-WAX capillary column (0.25 mm × 30 m). The performance of the EC reactor system using different catalysts are reported and analyzed by Equations (1) and (2) product yield (μmol.cm⁻².L⁻¹) and Faradaic efficiency (%), respectively.

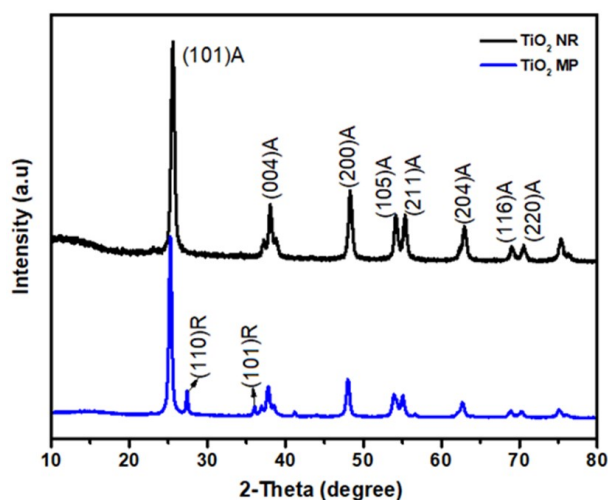


Figure 2. XRD pattern of TiO₂ nanorods (NR) and microparticle (MP) catalyst samples. *A = anatase and R = Rutile.

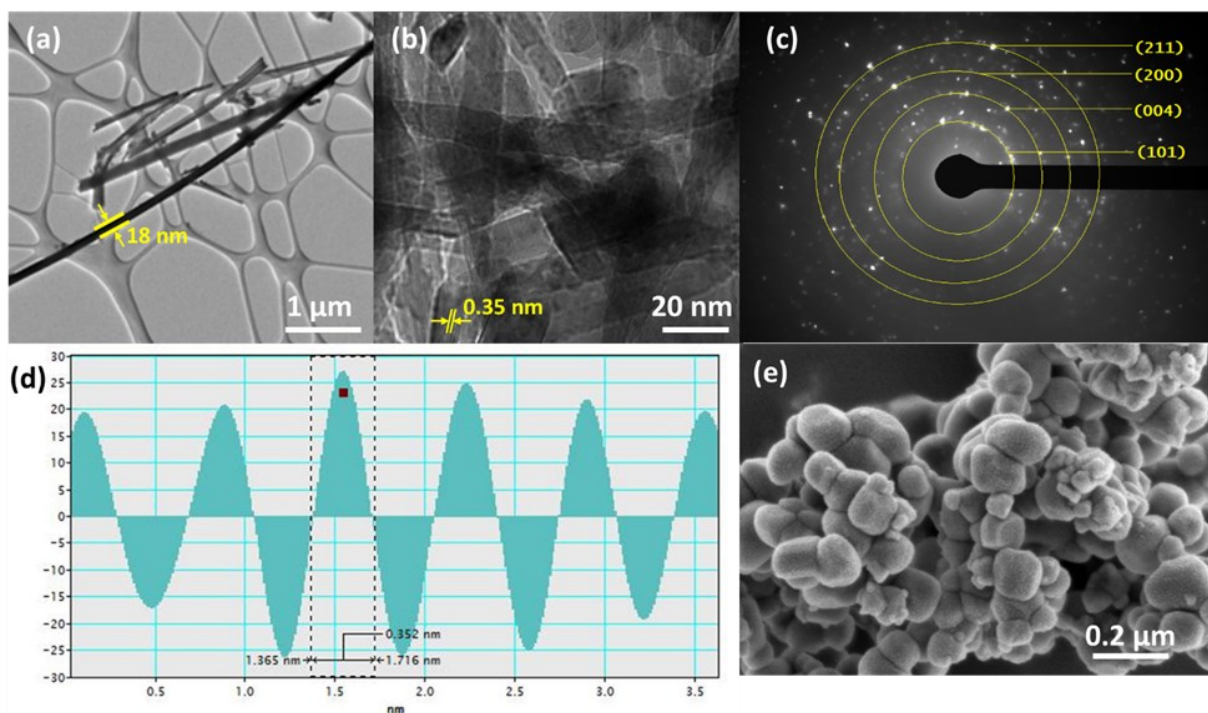


Figure 3. (a-b) HR-TEM micrographs of TiO₂ nanorods (NR), (c) SAED pattern of TiO₂ NR, (d) observed d-spacing value for TiO₂ NR and (e) FESEM of TiO₂ microparticle (MP) electrocatalyst.

$$\text{Product Yield} = \frac{\text{moles of Product}}{\text{Electrode area} \times \text{Volume of reactor}} \quad (1)$$

$$\text{Faradaic Efficiency (FE)} = \frac{\varepsilon \times n \times F}{Q} \times 100 \quad (2)$$

3. Results and Discussion

3.1 Characterization of Electrocatalysts

The X-ray diffraction patterns of TiO₂ NR and TiO₂ MP electrocatalyst samples, calcined at 500 °C up to 5 h are shown in Figure 2. The peaks for TiO₂ NR and MP were indicated at 2-theta (degree) 25.4°, 38.0°, 48.1°, 53.0°, 55.2° and 62.9°, which corresponds to (101), (004), (200), (105), (211) and (204) planes associated with tetragonal anatase, all in pure anatase phase. However, in TiO₂ MP diffraction patterns additional peaks at 27.4° and 36.07° can be seen, which corresponds to (110) and (101) planes associated with rutile phase [27]. Similar XRD peaks were reported by Steky *et al.* [28] for the nanostructured titania via alkaline hydrothermal treatment using ammonia solution with the presence of anatase and trace of rutile phases. It can be concluded that the TiO₂ NR structure in pure anatase phase can be acquired via hydrothermal method using NaOH as alkaline agent.

HR-TEM micrographs and FESEM of TiO₂ nanorods (NR) and TiO₂ microparticle (MP) electrocatalysts are depicted in Figure 3a-e. In Figure 3a, the HR-TEM micrographs of TiO₂ nanorods (NR) shows the formation of nanorod structures with approximately 6-8 micrometers in length and 18 nm in diameter. Figure 3b shows d-spacing of 0.35 nm which corresponds to the (101) facet of TiO₂ anatase phase. The value of d-spacing was observed by using DigitalMicrograph®, Gatan Inc. software tool, as shown in Figure 3d. From the SAED patterns as depicted in Figure 3c, the crystal interplanar spacings corresponding to diffraction rings/facets starting from inner side to outwards were (101), (112), (211), and (220). The FESEM micrograph of TiO₂ microparticle is also depicted in Figure 3e, where we can observe the TiO₂ particles are in micro-spherical form. However, HR-TEM micrographs confirms the formation of TiO₂ nanorod structure of hydrothermally synthesized electrocatalyst.

The N₂ adsorption and desorption isotherms of the calcined TiO₂ NR and TiO₂ MP are shown in Figure 4. Both microparticle and nanorods show increase in N₂ absorption above 0.9 partial pressure (P/P₀). Furthermore, N₂ adsorption-desorption isotherms revealed mesoporous structure for TiO₂ NR with hysteresis

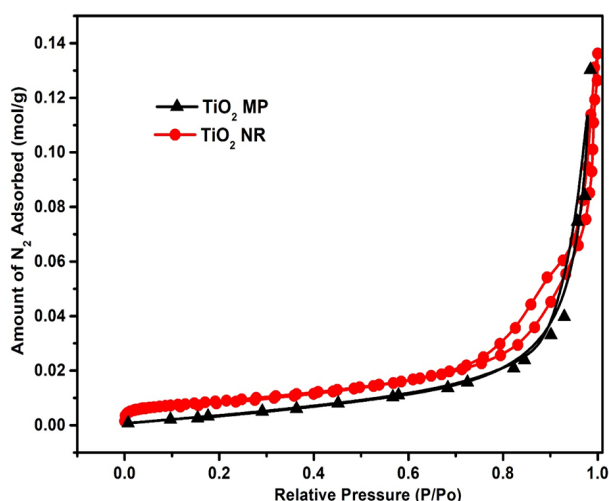


Figure 4. N₂ adsorption-desorption isotherms of TiO₂ NR and TiO₂ MP electrocatalyst.

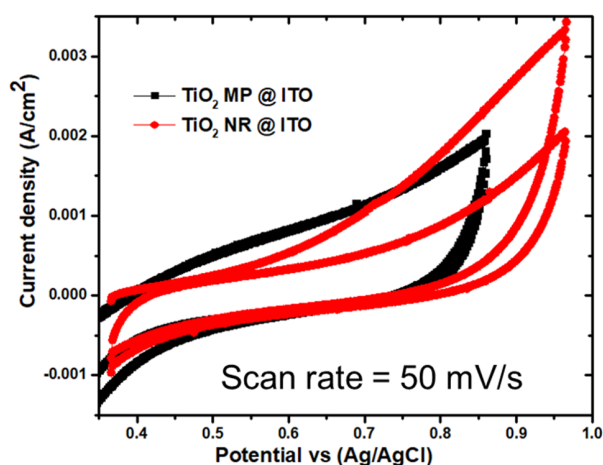


Figure 5. Cyclic voltammetry curves for various electrodes/electrocatalyst @50 mV/s and 0.3 to 1.0 V vs Ag/AgCl potential range.

Table 1. Summary of structural properties TiO₂ NR and TiO₂ MP electrocatalyst samples.

Catalyst	BET _{SA} (m ² /g)	Pore radius (nm)	Pore volume (cm ³ /g)
TiO ₂ MP	25.43	9.70	0.15
TiO ₂ NR	50.26	12.72	0.31

*SA = Surface Area

loop of type IV according to IUPAC. The summary of structural properties including BET surface area, pore volume and pore size/radius of TiO₂ MP and TiO NR are presented in Table 1. The BET surface area of TiO₂ MP was 25.43 m²/g, pore volume 0.15 cm³/g and pore radius 9.70 nm were recorded. However, BET surface area of hydrothermally modified TiO₂ NR was recorded as 50.62 m²/g which is higher than unmodified commercial TiO₂ MP catalyst sample. Similar trends were observed in the pore volume 0.31 cm³/g and pore radius 12.72 nm of TiO₂ NR, which were recorded higher as compared to TiO₂ MP. The significant increments in structural properties of modified TiO₂ NR was obtained through simple hydrothermal treatment and these structural properties of TiO₂ NR might enhance the electrocatalytic performance.

The measurement of cyclic voltammetry (CV) curve at 50 mV/s scan rate within a potential range ~ 0.3 to 1.0 V vs Ag/AgCl was per-

formed for different samples and depicted in Figure 5. The CV tests shows relatively higher electrochemical surface area and current density for TiO₂ NR electrocatalyst as compared to other samples. This increment is desirable for enhanced electrocatalytic activity towards CO₂ reduction for methanol and direct water electrolysis for H₂ production. It can be observed from the cyclic voltammetry curves the current density of TiO₂ NR increases with the increase in the applied potential. It shows that with increase in the applied potential the current density increases, which results in the enhanced electrocatalytic reactions for methanol formation and H₂ production at electrode-electrolyte interface. The present cyclic voltammetry data is consistent with reported literature for electrocatalytic activity for CO₂ reduction [21].

3.2 Electrocatalytic CO₂ Reduction

To analyze the direct water electrocatalysis for H₂ production and CO₂ reduction for methanol production under 2 V of applied potential using three electrode system. An online gas chromatography (GC-TCD, Agilent 6890) equipped with Carbon plot column was used to analyze the gas products and an offline liquid GC-FID (Agilent, 7820A) equipped with DB-WAX column was used to analyze liquid products. In outlet product gas mainly H₂ was observed and in the liquid methanol was detected. Figure 6a shows the electrocatalytic activity test for different electrodes. As we can observe from the experiments that TiO₂ NR electrocatalyst showed highest catalytic activity in terms of H₂ and methanol production. The H₂ and methanol production rate for modified

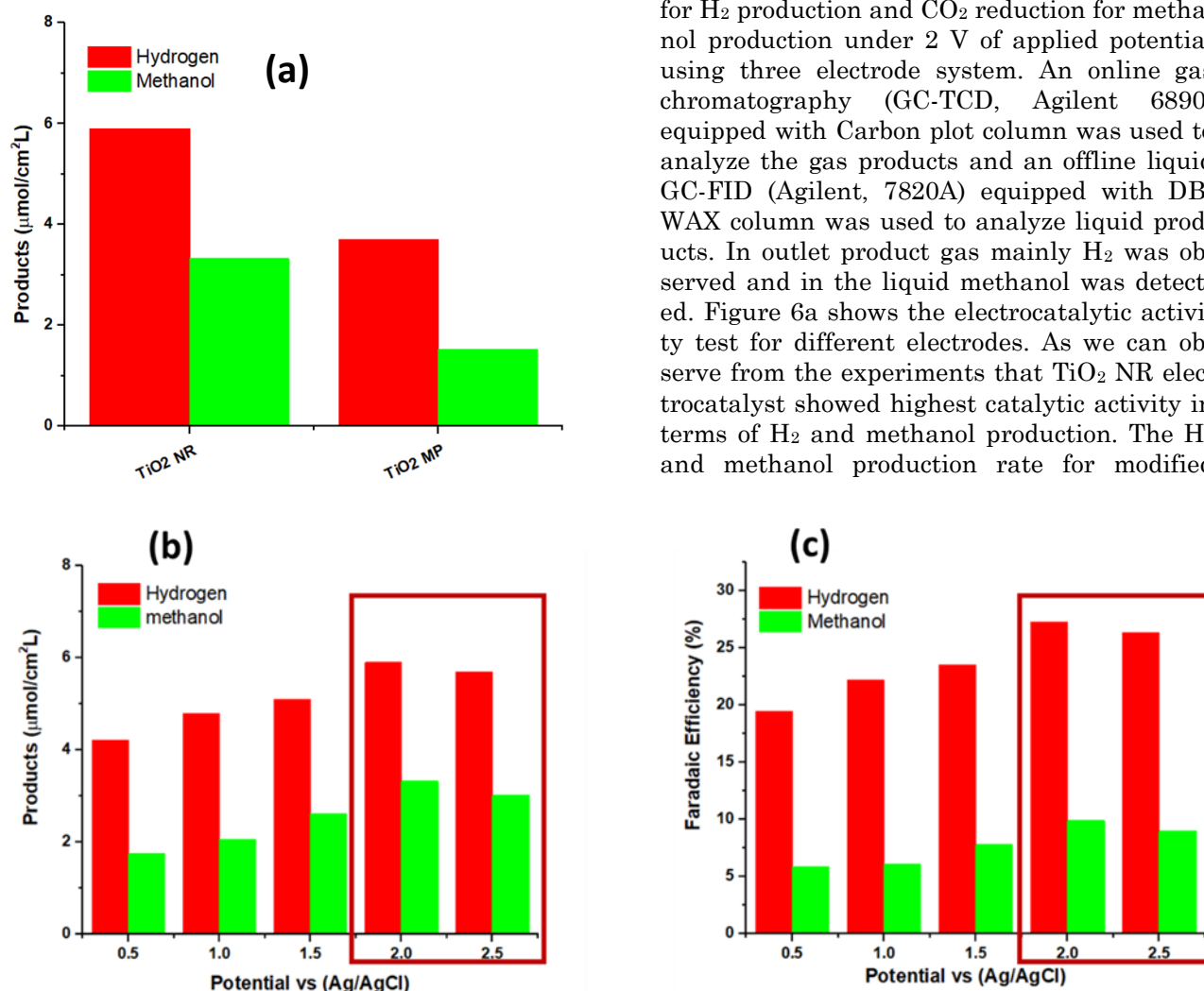


Figure 6. (a) Electrocatalytic activity test for different electrocatalysts (b-c) electrocatalytic activity of TiO₂ NR electrocatalyst under different electric potentials.

TiO₂ NR electrocatalyst at 2 V of potential vs Ag/AgCl for 1 h was recorded as $\sim 6.0 \mu\text{mol} \cdot \text{cm}^{-2} \cdot \text{L}^{-1}$ and $3.32 \mu\text{mol} \cdot \text{cm}^{-2} \cdot \text{L}^{-1}$, respectively. The electrocatalytic activity of TiO₂ NR electrocatalyst was further investigated under different applied electric potentials (0.5–2.5 V), as depicted in Figure 6b and 6c. As shown in the results, product yield and faradaic efficiency for methanol and H₂ production increased gradually from 0.5 V to 2.0 V applied potentials. However, a slight decline in methanol and H₂ production rate and faradaic efficiency can be absorbed at 2.5 V applied potential. The decline in product generation and faradaic efficiency might be due to overpotential that causes excess concentration of H⁺/or OH⁻ species around electrodes. These excess H⁺/or OH⁻ species causes hindrance for CO₂ adsorption on catalyst surface that results in decline in production rate and faradaic efficiency. Huang *et al.* [29] also reported similar trend for product generation in electrocatalytic CO₂ reduction to methanol.

The improvement in product yields of methanol and H₂ was mainly due to the notable improvements and modification in morphology of

TiO₂ electrocatalyst interface. Moreover, the improvements in catalytic activity of TiO₂ NR electrocatalyst might be due to enhanced charge separation for TiO₂ after surface modification. The cyclic voltammetry (CV) results for TiO₂ NR electrocatalyst also provide justification for the enhanced catalytic activity.

3.3 Electrocatalytic Mechanism of CO₂ Reduction

On the basis of available related literature and experiments, we propose a hypothetical reaction mechanism for electrocatalytic CO₂ reduction to methanol and H₂ over TiO₂ NR electrocatalyst. The schematics of proposed reaction mechanism is shown in Figure 7. In the first step, the oxidation of electrolyte/water containing OH⁻ occurs at anode side. After losing electron to anode proton/H⁺ produced at anode side and due to concentration gradient, these protons/H⁺ migrate towards cathode side. At cathode side, after bubbling and dissolving CO₂ through electrolyte, molecules of dissolved CO₂ start to adsorb at electrocatalyst by creating a complex [TiO₂ NR-CO₂]⁺ via interaction of

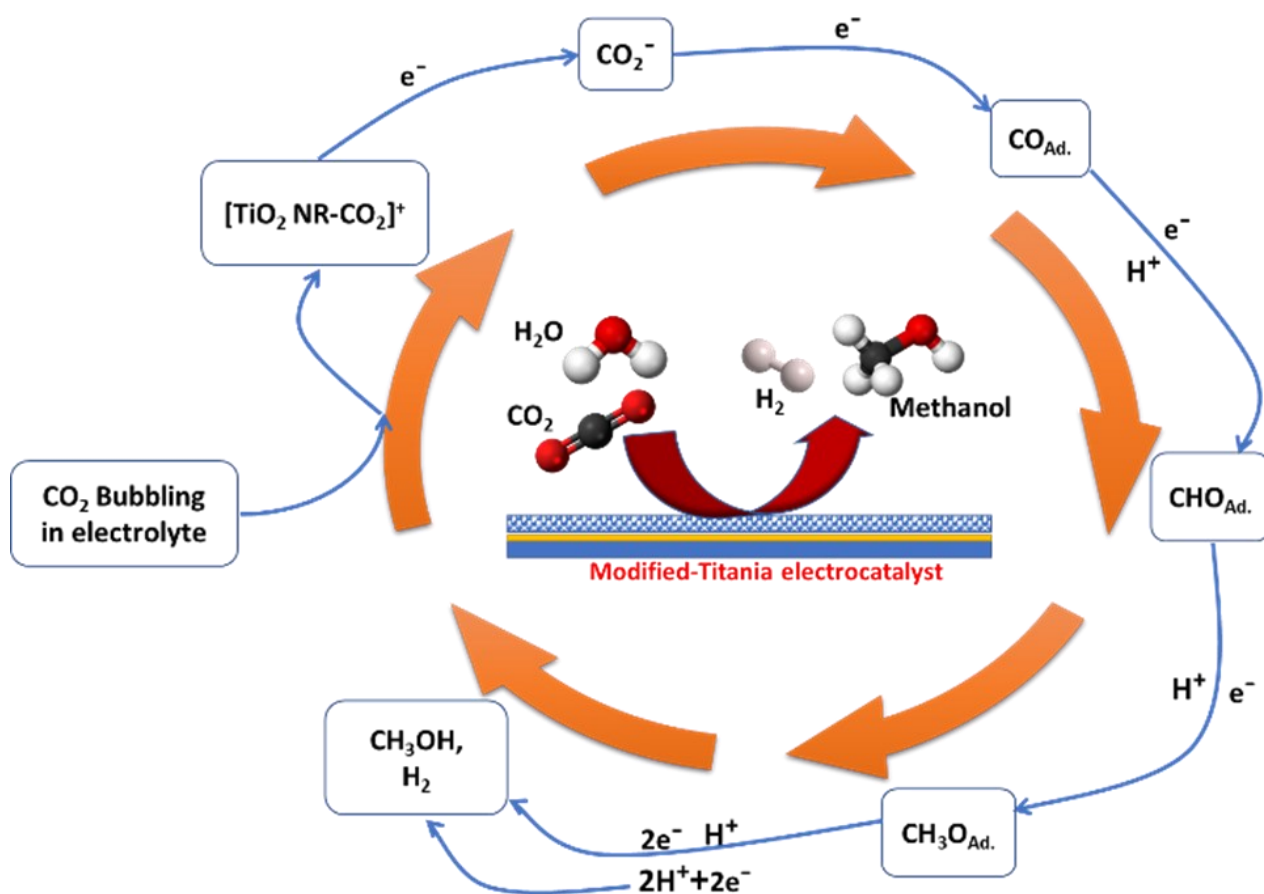
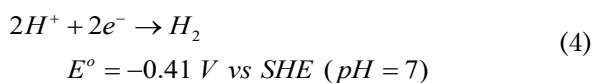
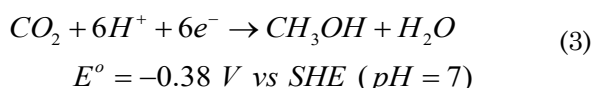


Figure 7. Schematic reaction mechanism for electrocatalytic CO₂ reduction over TiO₂ NR.

hydrogen between molecules. After adsorption of CO₂ complex on electrocatalyst, the CO₂ molecule convert into CO₂⁻ after reduction process. The reduced CO₂⁻ molecule further transfer second electron to convert into intermediate CO or adsorbed CO/CO_{Ad}. After that, third transfer of electron occurs along with proton/H⁺ to convert CO_{Ad} into adsorbed CHO or CHO_{Ad} intermediate. Further, electron and proton/H⁺ transfer leads to conversion of CHO_{Ad} into intermediate CH₃O or adsorbed CH₃O_{Ad} intermediate. In final step, the last electron and proton/H⁺ is transferred to the CH₃O_{Ad} and methanol is produced at electrocatalyst. Also, two protons/H⁺ react with two electrons to produce 1 mole of hydrogen. The overall reaction is shown in Equations (3) and (4).



4. Conclusions

The synthesized ITO sheet decorated with TiO₂ NR electrocatalyst can efficiently boost charge separation and surface area to improve the methanol and H₂ production rates for CO₂ reduction and direct water electrocatalysis during the EC reaction. The TiO₂ NR electrocatalyst catalysts exhibit excellent EC CO₂ reduction and water electrolysis activity with methanol production value of 3.32 μmol.cm⁻².L⁻¹ and H₂ production value of 6 μmol.cm⁻².L⁻¹ under 2.0 V of applied electric potential. The CV experiments for TiO₂ NR electrocatalyst also confirms the justification for the improved catalytic performance. This work develops an effective and facile TiO₂ NR electrocatalyst as a competent EC working electrode for sustainable energy conversion.

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